

Zero Ammonia Slip Technology for Combined Cycle Gas Turbine Exhaust



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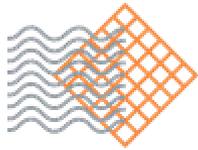
Outline

- **Introduction**
- **Zero-Slip™ Technology Description**
- **Pilot Test Results**
- **7 MW Commercial Demonstration**
- **Conclusions**

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Introduction

- **Selective Catalytic Reduction (SCR)**
 - Vanadia-Titania SCR Catalyst in Path of Flue Gas
 - “Honeycomb” Monolith with Channels for Gas Flow
 - Ammonia Reductant (NH_3) Injected Upstream of Catalyst
 - NO_x Reactant in Flue Gas (NO_x is an Ozone Precursor)
 - Reduction of NO_x to N_2 and H_2O (“de- NO_x Reaction”)
 - High Conversion of Flue Gas NO_x to Products
 - Permit Outlet NO_x Levels Typically 2-10 ppm
- **Outlet Ammonia is Termed Ammonia Slip**
 - Non-Stoichiometric Local Conditions Across Catalyst
 - Flue Gas Flow Non-Uniformities
 - NH_3 Injection Grid Tuning to Match Flue Gas Flow
 - Inadequate Mixing Time
 - Ammonia Slip Permit Levels
 - Typically 2-10 ppm or even 30 ppm

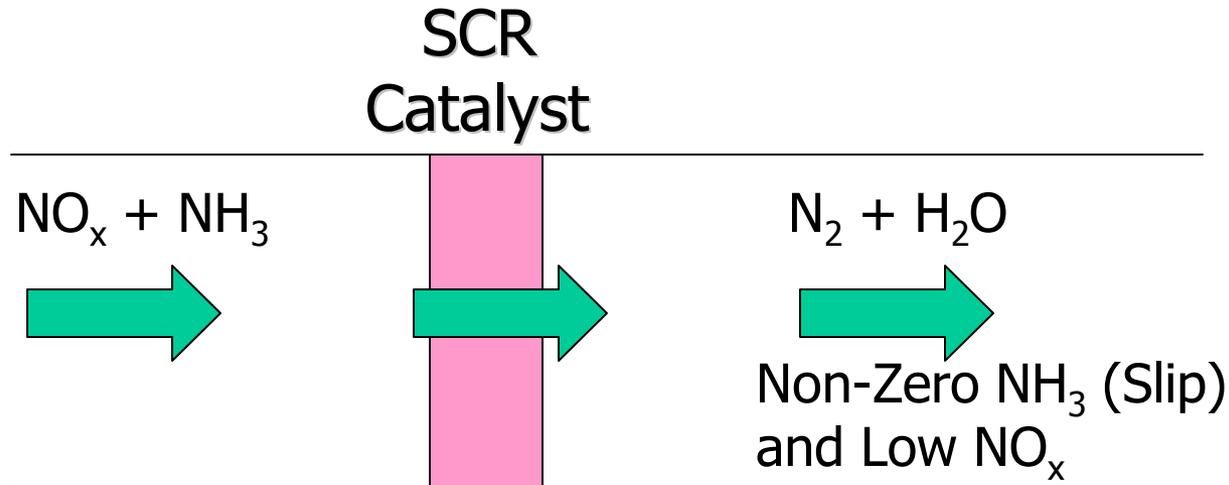
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SCR NO_x Reduction – de-NO_x Reactions



NO_x Reduction Over SCR Catalyst



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Zero-Slip™ Technology - Purpose

- **Ammonia Slip is Regulated in Some Localities**
 - NH₃ is not a Criteria Pollutant (Federal)
 - Toxic Air Contaminant under SCAQMD Rule 1401
 - Some Local Permit Agencies Require Control of NH₃ Slip
- **Local Regulations Have Tightened**
 - NO_x < 2 – 5 ppm
 - NH₃ Slip < 2 – 3.5 ppm
- **NH₃ Salt Formation Reactions Contribute to PM**
 - $2 \text{NH}_3 + \text{H}_2\text{SO}_4 \rightarrow (\text{NH}_4)_2\text{SO}_4$
 - $\text{NH}_3 + \text{HNO}_3 \rightarrow \text{NH}_4\text{NO}_3$
 - NH₃ Sources
 - Fertilizers
 - Animal Feeding Operations
 - SCR and SNCR Ammonia Slip (Relatively Small)
- **Regional Haze**

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Zero-Slip™ Technology - Description

- **Enhanced SCR Technology for Combined Cycle Gas Turbines to Achieve down to “Zero” NH₃ Slip**
- **Mitsubishi/Cormetech Joint Development**
 - Patented
 - Demonstrated Commercially
- **General Features**
 - Standard SCR Catalyst and Zero-Slip™ Catalyst Layers
 - Zero-Slip™ Catalyst Composition is Proprietary
 - NH₃ Injection Above Stoichiometric
 - Promotion of Good Mixing
 - Destruction of Ammonia over Zero-Slip™ Catalyst
 - Can Achieve Down to “Zero” Ammonia at the Outlet
 - Applicable to New Units and Retrofits

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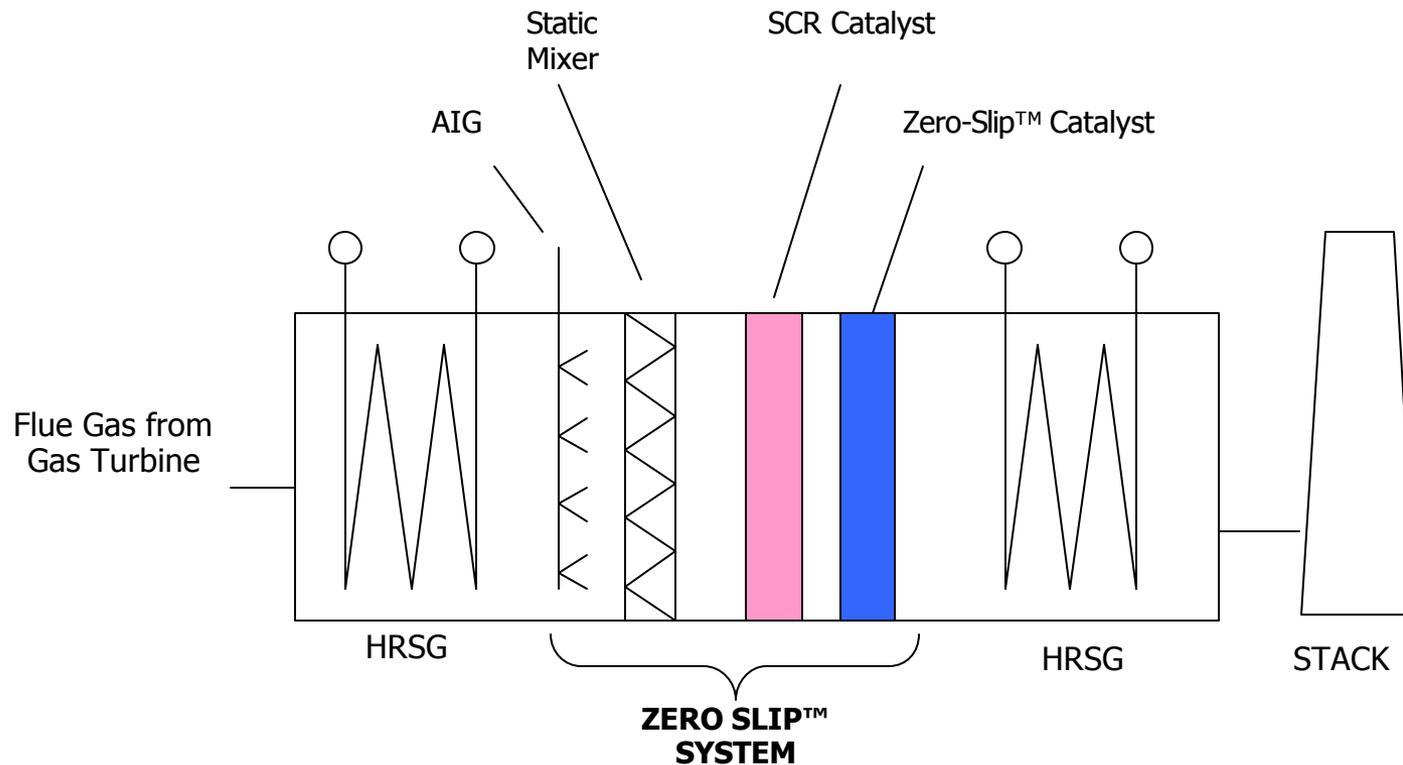
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Zero-Slip™ Technology

Schematic Drawing for Typical Split Heat Recovery Steam Generator (HRSG)



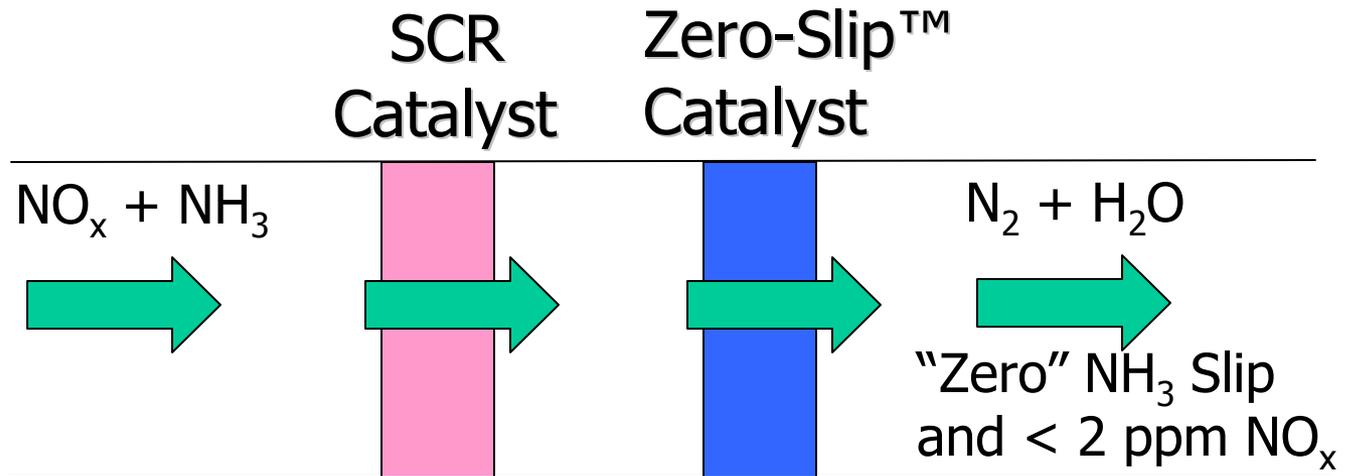
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Zero-Slip™ Technology – Reactions



NO_x Reduction Over SCR Catalyst



De- NO_x and NH_3 Destruct Over Zero-Slip™ Catalyst



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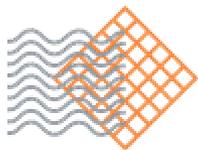
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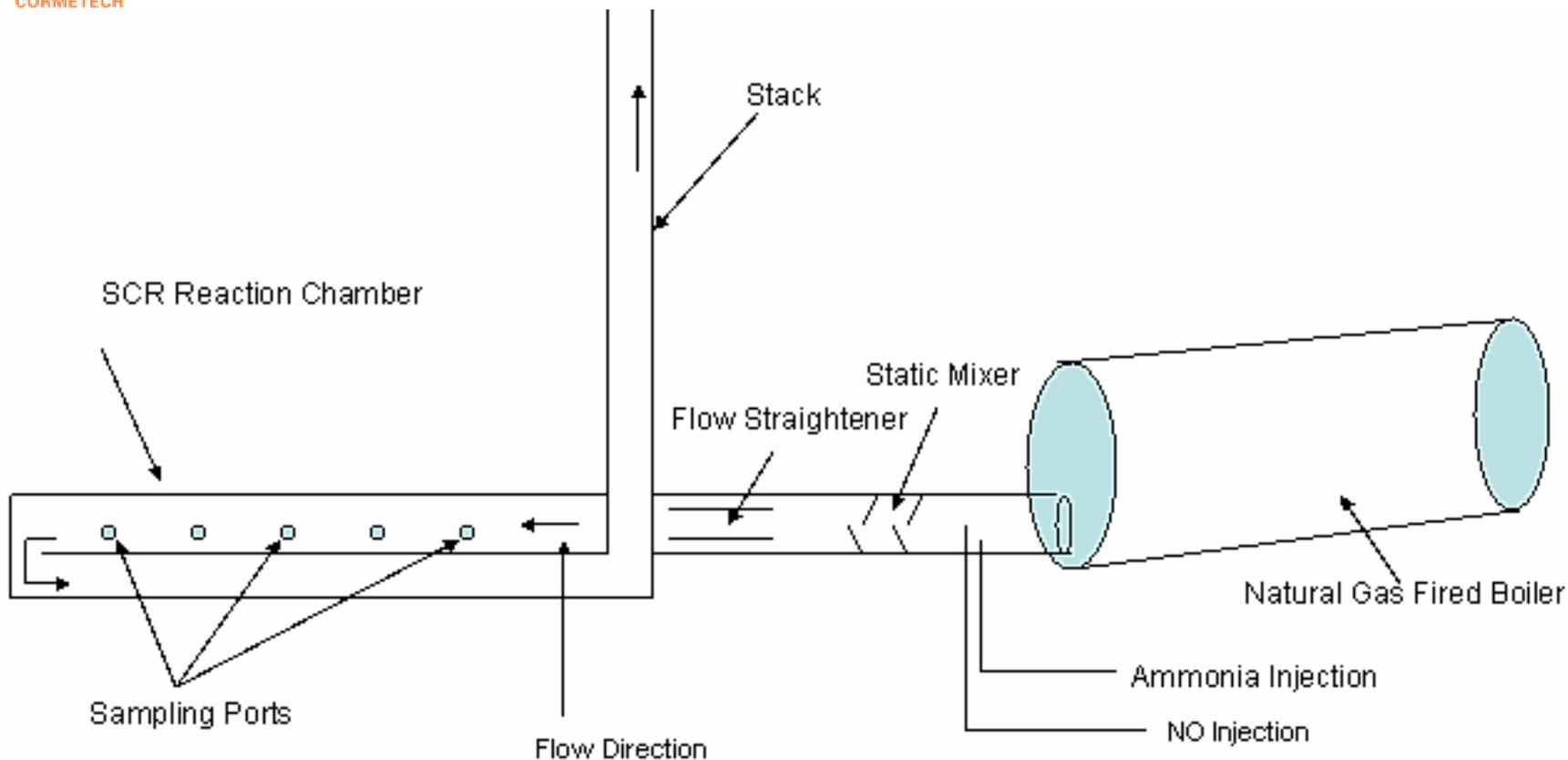
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Zero-Slip™ Technology Pilot Reactor



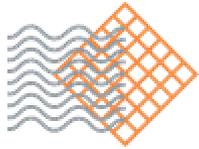
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Zero-Slip™ Technology

Pilot Study - Test Conditions

Target Test Condition Number	1	2	3	4	5
NO _x Inlet Concentration (ppmvdc)	32	32	32	32	32
O ₂ Concentration (volume %)	12.4	12.4	12.4	12.4	12.4
H ₂ O Concentration (volume %)	10.7	10.7	10.7	10.7	10.7
Superficial Gas Velocity (Nm/s)	1.23	1.23	1.23	1.23	1.23
Gas Flow (SCFM)	61.9	61.9	61.9	61.9	61.9
NH ₃ /NO _x Molar Ratio	0.80	0.90	1.14	1.23	1.60

Flue Gas Flow ?



?



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Layer 1
SCR Catalyst

Layer 2
Zero-Slip™ Catalyst

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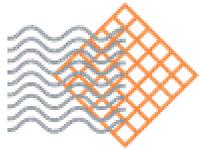
Pilot Study - Test Results – NH₃ Slip < 0.1 ppm

NH ₃ /NO _x Molar Ratio (Inlet)	Temperature (°C)	Ammonia Slip by FTIR (ppmvdc)	Outlet NO _x by FTIR (ppmvdc)	Estimated NO _x Conversion (%)
0.81	316	0.01	2.3	96%
0.95	316	0.07	0.8	99%
1.14	316	0.02	1.2	98%
1.23	316	0.02	1.4	97%
1.60	316	0.01	2.3	96%
0.79	350	0.01	5.7	90%
0.93	350	0.04	1.0	98%
1.18	350	0.01	1.8	97%
1.27	350	0.01	2.1	96%
1.52	350	0.01	1.8	97%

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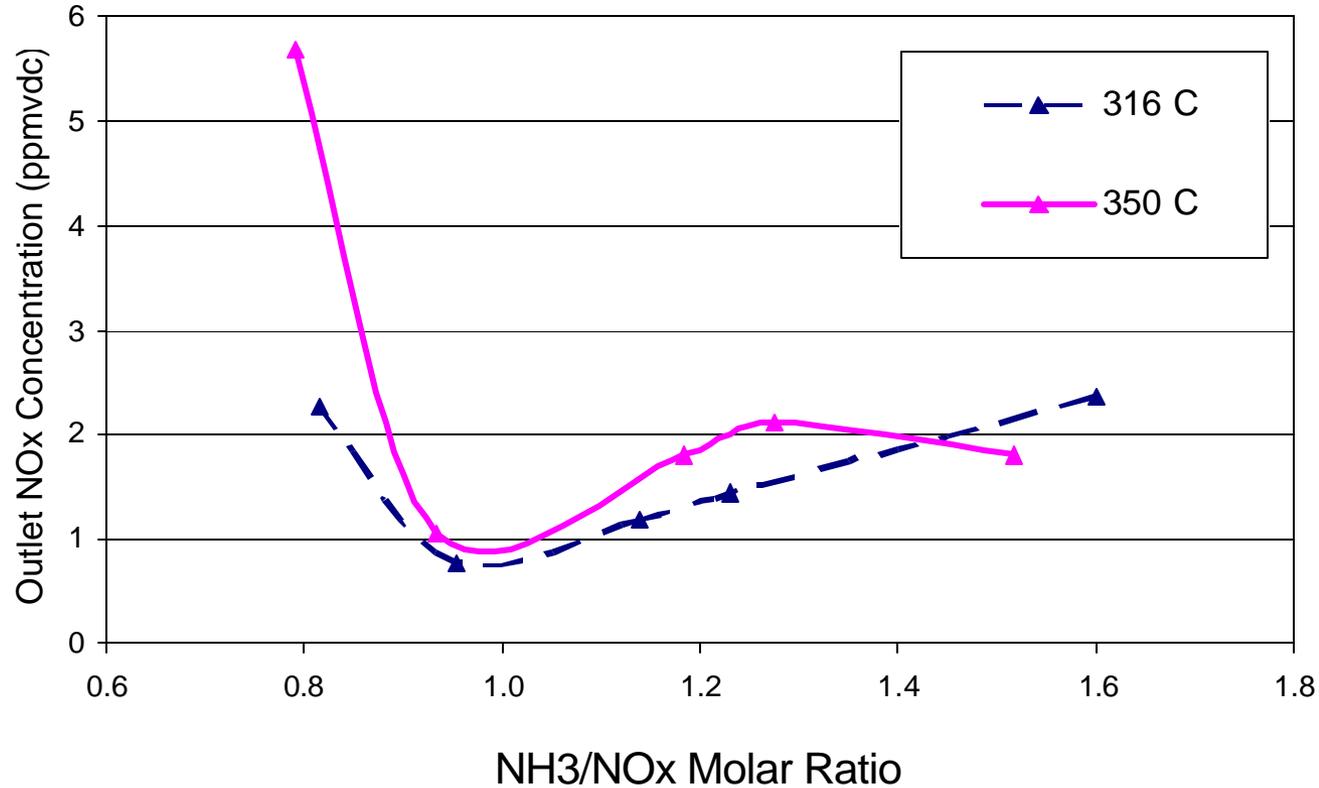
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Zero-Slip™ Technology

Pilot Study - Test Results for Outlet NO_x



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Zero-Slip™ Technology

Commercial Demonstration



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- **Host: Paramount Petroleum Corp.**
- **Location: Los Angeles Basin**
- **Unit: 7 MW Cogeneration**
- **Startup: January 2003**



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Commercial Demonstration

Initial Performance at Startup - Test Conditions

Gas Turbine Load (MW)	5	5	5
Flue Gas Temperature (°C)	355	355	355
Flue Gas Temperature (°F)	670	670	670
Inlet Oxygen (vol. %, dry)	13.1	13.1	13.1
NH ₃ /NO _x Molar Ratio	0.8	1.1	1.8

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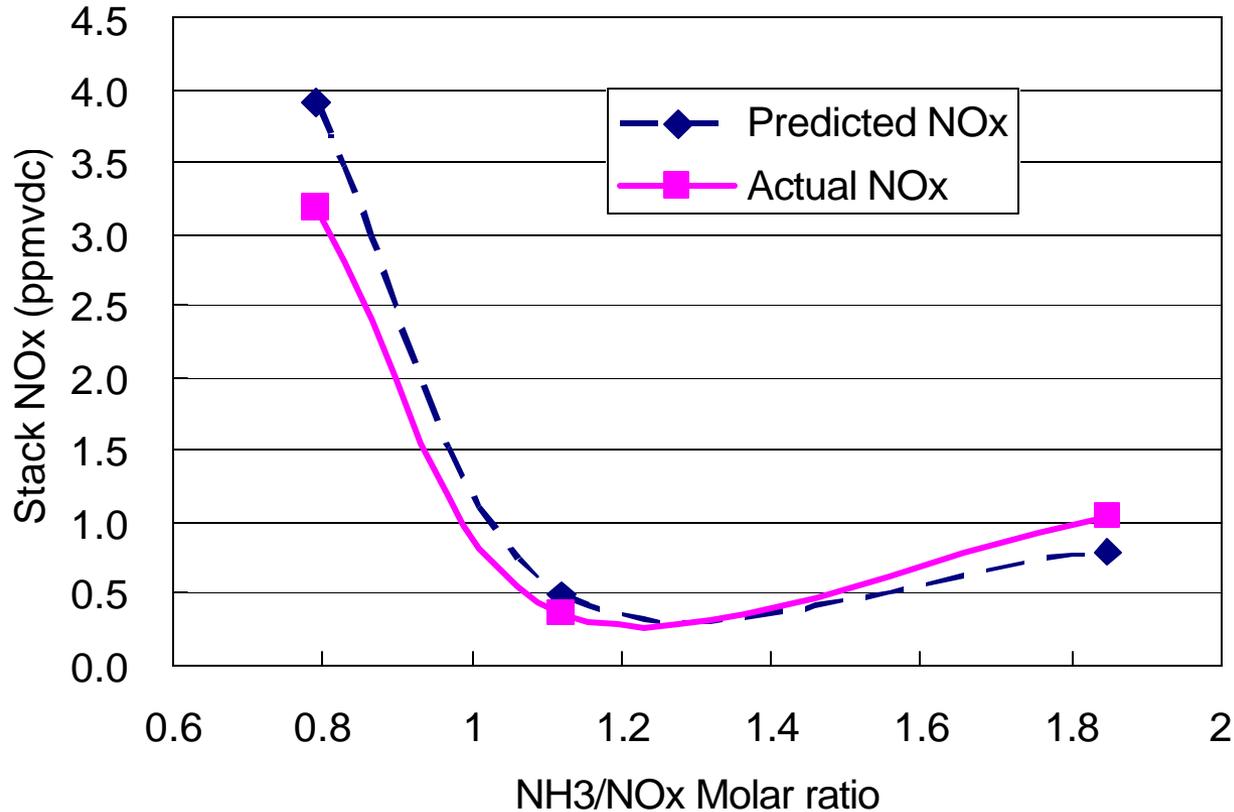
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Commercial Demonstration

Initial Performance at Startup – NO_x vs. Molar Ratio



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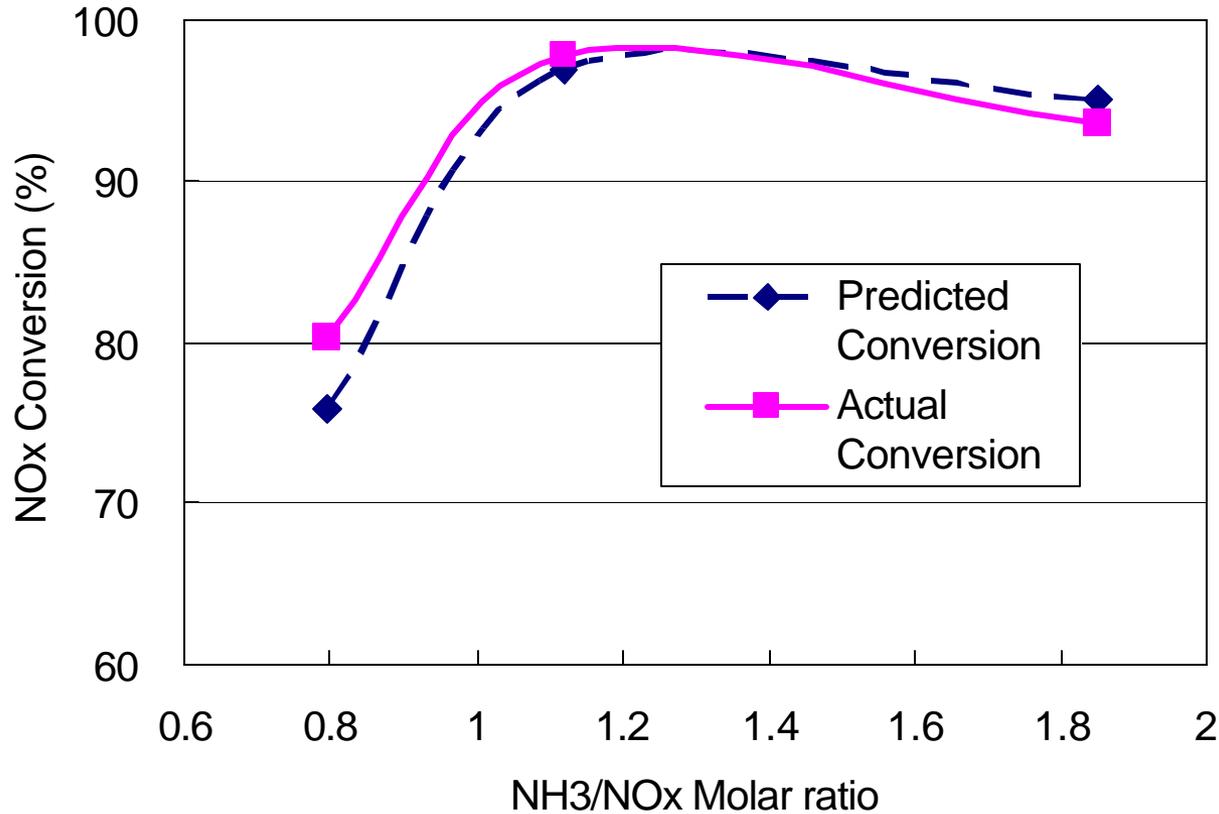
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Commercial Demonstration

Initial Performance – NO_x Conversion vs. Molar Ratio



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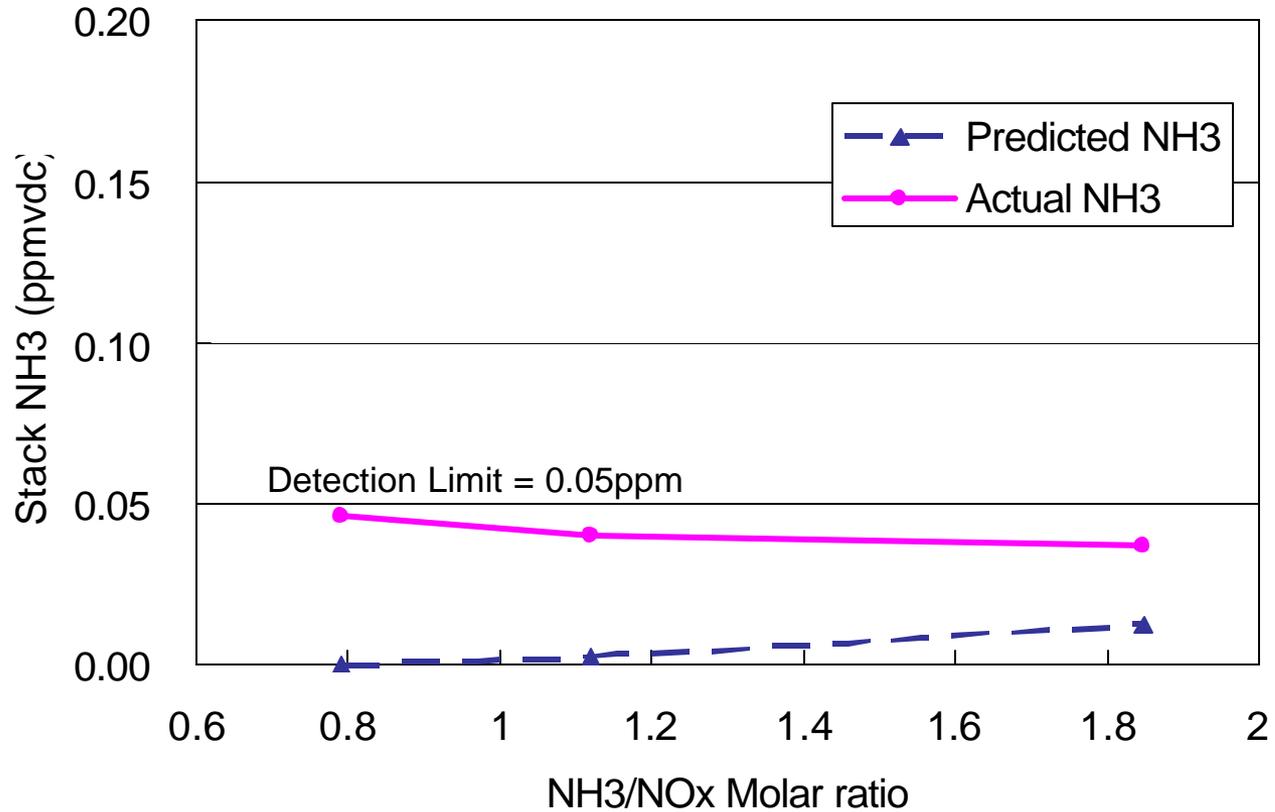
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Commercial Demonstration

Initial Performance – NH₃ Slip vs. Molar Ratio



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Commercial Demonstration

Performance Results after 3000+ Hours

Gas Turbine Load (MW)	5	5
Flue Gas Temperature (°C)	322	324
Flue Gas Temperature (°F)	611	615
Inlet Oxygen (vol. %, dry)	14.8	14.8
NH ₃ /NO _x Molar Ratio	0.9	1.3
Outlet NO _x (ppmvdc)	1.5	0.4
Outlet NH ₃ (ppmvdc)	Less than detection limit	0.10 (at detection limit)

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Zero-Slip™ Technology - Conclusions

- **A Commercial Zero-Slip™ System has been Successfully Operated for over 8 Months**
 - Achieved Ammonia Slip < 0.1 ppm (Effectively “Zero”)
 - Achieved High NO_x Reduction Levels and Low Outlet NO_x
 - ~0.5 ppm NO_x Outlet Concentration Initially
 - 2.0 ppm NO_x Outlet Concentration Expected at End of Life
- **The Design Model Accurately Predicted Scale-Up**
- **Zero-Slip™ Systems are Available Commercially**
 - Applicable to Combined Cycle Gas-Fired Units
 - New and Retrofit
 - System Design is Flexible to Meet Customer Needs
 - Extremely Low NO_x Levels, and/or
 - Extremely Low Ammonia Slip

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Acknowledgements

- **Paramount Petroleum Corp. – for providing the host site for the commercial demonstration**
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